Application No. 10/584,758 Docket No.: 13156-00058-US1

Amendment dated February 12, 2008 Reply to Office Action of December 31, 2007

## AMENDMENTS TO THE CLAIMS

This listing of claims will replace all prior versions and listings of claims in the application.

Claims 1-5. (Cancelled)

6. (Currently Amended) A process for preparing butadiene from n-butane comprising:

A) providing a feed gas stream a comprising n-butane;

 feeding the feed gas stream a comprising n-butane into at least one first dehydrogenation zone and nonoxidatively catalytically dehydrogenating n-butane

to obtain a product gas stream b comprising n-butane, 1-butene, 2-butene, butadiene, hydrogen, low-boiling secondary constituents and in some eases

optionally steam;

C) feeding the product gas stream b of the nonoxidative catalytic dehydrogenation

and an oxygenous gas into at least one second dehydrogenation zone and oxidatively dehydrogenating 1-butene and 2-butene to obtain a product gas stream

c comprising n-butane, 2-butene, butadiene, hydrogen, low-boiling secondary

constituents and steam, said product gas stream c having a higher content of

butadiene than the product gas stream b;

D) removing hydrogen, the low-boiling secondary constituents and steam to obtain a

C<sub>4</sub> product gas stream d substantially consisting of n-butane, 2-butene and

butadiene;

E) separating the C<sub>4</sub> product gas stream d into a recycle stream e1 consisting

substantially of n-butane and 2-butene and a stream e2 consisting substantially of

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butadiene by extractively distilling and recycling the stream el into the first dehydrogenation zone;

optionally, feeding some or all of the stream e2 consisting substantially of

butadiene into a selective hydrogenation zone and selectively hydrogenating

butadiene to 1- and/or 2-butene to obtain a stream f comprising 1-butene and 2-

butene;

F)

G) optionally, when F is carried out, feeding the stream f comprising 1-butene and 2-

butene into a distillation zone and removing a product of value stream gl

consisting substantially of 1-butene to leave a stream g2 comprising 2-butene;

H) optionally, when F and G are carried out, recycling the stream g2 comprising 2-

butene into the first dehydrogenation zone.

7. (Currently Amended) The process according to claim 6, wherein the noncatalytic nonoxidative

catalytic dehydrogenation of n-butane is carried out autothermally.

8. (Previously Presented) The process according to claim 6, wherein the feed stream a containing

n-butane is obtained from liquefied petroleum gas (LPG).

9. (Previously Presented) The process according to claim 6, wherein the extractive distillation is

carried out using N-methylpyrrolidone as an extractant.

10. (Previously Presented) The process according to claim 6, wherein F) and G) are carried out.

11. (Previously Presented) The process according to claim 6, wherein F), G) and H) are carried

out.

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